

Article

Carnot Battery Based on Brayton Supercritical CO₂ Thermal Machines Using Concentrated Solar Thermal Energy as a Low-Temperature Source

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Abstract: Carnot batteries store surplus power as heat. They consist of a heat pump, which upgrades a low-temperature thermal energy storage, a high-temperature storage system for the upgraded thermal energy, and a heat engine that converts the stored high-temperature thermal energy into power. A Carnot battery is proposed based on supercritical CO₂ Brayton thermodynamic cycles. The low-temperature storage is a two-tank molten salt system at 380 °C/290 °C fed by a field of parabolic trough collectors. The high-temperature storage consists of another two-tank molten salt system at 589 °C/405 °C. Printed circuit heat exchangers would be required to withstand the high pressure of the cycles, but shell and tube heat exchangers are proposed instead to avoid clogging issues with molten salts. The conventional allocation of high-temperature molten salt heat exchangers is then modified. Using solar energy to enhance the low-temperature thermal source allowed a round-trip efficiency of 1.15 (COP of 2.46 and heat engine efficiency of 46.5%), thus increasing the stored power. The basic configuration has a levelised cost of storage of USD 376/MWh while replacing the shell and tube heat exchangers with hybrid printed circuit heat exchangers is expected to lower the cost to USD 188/MWh.

Keywords: Carnot batteries; Brayton supercritical CO₂ thermodynamic cycle; high-temperature heat pump; pumped thermal energy storage; thermal energy storage; renewable energies dispatchability

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1. Introduction

The growing share of non-dispatchable renewable sources (mainly photovoltaic and wind) in the electricity mix due to decarbonisation measures must be supported by large storage systems capable of avoiding curtailments. Different technologies can be used to store electricity [1], each with different performances, as shown in Table 1. Pumped hydro-storage (PHS), gravity energy storage (GES), and compressed air energy storage (CAES) require specific geographical conditions, whereas liquid air energy storage (LAES), lithium-ion batteries (Li-Ion B), flow batteries (Flow B), and pumped thermal energy storage (PTES) do not. The present work deals with PTES, which is situated among the lower costs per stored energy (comparable with PHS) and has the lowest cost per unit of installed capacity. Regarding power-to-power (P2P) efficiency (also known as round-trip efficiency), PTES exhibits intermediate-high values, just behind Li-Ion B and, again, close to PHS, with an intermediate lifetime comparable to LAES. In summary, and according to

[1], PTES is a promising technology compared with others due to its high P2P efficiency, low specific costs, and no specific geographical requirements.

Table 1. Comparison of different electrical energy storages [1].

Technology	Energy density [kWh/m ³]	Energy cost [\$/kWh]	Energy cost [\$/kW]	P2P [%]	Lifetime [years]
PHS	0.5–1.5	5–100	300–5200	65–87	30–60
GES	0.5–1.5	N/A	N/A	70–86	30–40
CAES	1–12	2–200	400–2250	40–95	20–60
LAES	50	260–530	500–3500	40–85	20–40
Li-Ion B	300	500–2500	270–1500	85–95	5–15
Flow B	16–60	120–1000	175–10000	57–85	5–15
PTES	0.25–6.9	62–107	533–627	70–80	25–30

From a formal point of view, Frate et al. [2] established that PTES belongs to the so-called “Carnot Batteries”, a term formulated in the “Annex 36 Carnot Batteries” within the framework of the Technology Collaboration Program (TCP) of the International Energy Agency (IEA). These authors defined the conventional PTES as a system consisting of a heat pump and a heat engine operating between two thermal storages, one at a low temperature and another at a high temperature. During the charge period, the heat pump consumes electricity from the grid, transferring heat from the low-temperature storage to the high-temperature one; during the discharge period, the heat from the high-temperature storage is supplied to the heat engine. Then, part of the heat is converted into electricity that is injected into the grid, and the rest is released to low-temperature storage. With this classical architecture, the round-trip efficiency reaches no more than 60% [1], with the maximum theoretical value being 100%. An improved arrangement is the so-called Thermally Integrated Pumped Thermal Energy Storage (TI-PTES), with one thermal source in either the heat pump or the heat engine [2]. Nevertheless, as Dumont et al. [3] mentioned, “a Carnot battery is a system primarily used to store electric energy”, and it should at least consist of an electric input and an electric output.

The TI-PTES typically incorporates low-grade waste heat recovery as a thermal source. Zhang et al. [4] analysed the effects of including waste heat recovery in a PTES, concluding that the highest efficiency is achieved with a low heat storage temperature of around 100 °C. Regarding the high heat storage temperature, if set to 130 °C, the round-trip efficiency reaches 66.52%. In terms of waste heat, the round-trip efficiency reaches 99.3% when the inlet temperature of the waste heat rises to 90 °C. Previous authors used organic Rankine cycles (ORC) as the technology for both the heat pump (vapour-compressed heat pump, VCHP, with compressor and valve) and the heat engine, which is a common approach in PTES and TI-PTES. Zhao et al. [5] analysed the role of recuperators in both cycles, concluding that if recuperators are not used, the levelised cost of storage can increase by 12%. Regarding the optimisation of costs, Frate et al. [6] carried out a multi-criteria economic analysis taking into account both the cost and efficiency of a TI-PTES based on a high-temperature (180 °C) heat pump and an ORC, both using R1233zd(E) as working fluid and waste heat at 80 °C/60 °C. They concluded that large systems (5 MW of charging power for 8 h of storage) may achieve an energy cost of 140 €/kWh and an investment of 2300 €/kW, with a round-trip efficiency of 60%.

The off-design operation has been analysed by Eppinger et al. [7] in an ORC-based system (VCHP and heat engine), both using R1233zd(E) as working fluid and a heat pump outlet temperature of around 100 °C. The heat leaks in the storage only slightly affected the round-trip efficiency, but the mass flow rate reduction strongly influenced the efficiency decrease. A yearly simulation in a small grid fed with photovoltaic energy was performed, showing that PTES is particularly useful in the period between winter and

summer, with similar demand and supplied photovoltaic energy. Frate et al. [8] also conducted a partial-load analysis with a TI-PTES where the thermal source comes from solar thermal collectors, leading to a high-temperature heat pump and an ORC, both operated with pentane. The temperature achieved by the solar field allows an average round-trip efficiency between 85% and 87%, with the system operating in various conditions, even in cold seasons. While the efficiency is nearly constant over the year, the charging and discharging hours, and thus the stored energy, is more than double from January to July.

Redelinghuys et al. [9] explored the interaction between stored solar thermal energy and imported PV renewable energy through electric heaters within a Carnot battery application in a conventional parabolic trough concentrating solar power (CSP) plant. In this case, the heat pump is replaced by the electric heaters. They found that curtailments in solar thermal energy take place for specific design parameters, leading to operational trade-offs in the Carnot battery.

Although PTES based on organic Rankine cycles (both heat pump and heat engine) are very common, other thermodynamic cycles such as Brayton and transcritical Rankine with CO₂ can also be found in the literature. Zhao et al. [10] investigated the economic feasibility of PTES, including Brayton cycles with solid and liquid reservoirs (sensible heat) and transcritical Rankine cycles with CO₂ and liquid reservoirs. The recuperated transcritical Rankine system with Therminol VP-1 as storage material reaches a maximum round-trip efficiency of 68%, with the lowest capital cost (209 M\$) for 50 MW and a discharge duration of 6 h. The lowest power and energy capital costs are 3790 \$/kW (for a discharge duration of 2 h) and 396 \$/kWh (for a discharge duration of 12 h), respectively. In another study, Zhao et al. [11] focused on optimising PTES based on transcritical cycles, analysing the influence of using recuperators and of the storage fluid. They found that recuperated options enhance the round-trip efficiency, reaching the highest efficiency (75.28%) with rapeseed oil as the storage medium. Regarding costs, the heat exchangers' share was the highest, up to 54%, while the highest share in storage reached up to 14%, and the costs of expanders and compressors ranged from 18% to 31% and 14% to 26%, respectively. The best economic performance was achieved using Therminol as the storage medium. A comparison between different cycles (Brayton, Brayton/Rankine, and transcritical Rankine with CO₂) and storage systems (packed bed, molten salts and water) was carried out by Steinmann et al. [12], including the concept of Compressed Heat Energy Storage (CHEST), which considers two Rankine cycles with latent and sensible storage.

Frate et al. [13] modelled the dynamics of a PTES based on closed Brayton cycles, studying the transient response and paying particular attention to the off-design operation. They found that the system can operate at partial load with negligible performance degradation and rapid transient response, which enables PTES for grid-scale applications.

Within the Brayton cycles, Rindt et al. [14] focused on recompression with supercritical CO₂, with a low pressure of 80 bar and a high pressure of 240 bar, ranging the temperature between 16 °C and 513 °C. They designed a unit of 3.5 MW of power output, reaching 38.9% of round-trip efficiency.

Novotny et al. [15] reviewed the commercial development of Carnot battery technology. They found a variety of systems, from the simplest charging with electrical resistors (replacing the heat pump by Joule effect) to more conventional systems using classical Rankine, transcritical Rankine with CO₂, ORC, and finishing with Brayton. The round-trip efficiency is usually below 70%, except when a low-temperature reservoir or a high-temperature source is available. Steger et al. [16] described a pilot plant of a pure PTES system based on ORC technology operated with R1233zd(E), which uses a water tank as thermal storage between 90 °C and 120 °C. The system is totally reversible, meaning that the compressor of the heat pump is the same unit as the expander of the heat engine. A similar research, but over the TI-PTES concept (waste heat as thermal source), was carried out by Eppinger et al. [17], including all the design processes with CAD models and steady-state simulation as a first step in building a pilot plant of 14.7 kW of charge power. CHEST

systems are also proposed to be tested, as described in Trebilcock et al. [18], where a numerical model in TRNSYS was created to analyse the efficiency and flexibility of the system when coupled to a smart district heating network. In the case of large units, PTES can be integrated with large-scale current thermal power plants, such as old coal plants or newer ones with supercritical Rankine power cycles. Thus, Blanquiceth et al. [19] analysed five alternatives based on a two-tank molten salt storage system. The round-trip efficiency is around 50% to 65%, reaching high energy and power density values. An argon heat pump is recommended for the Rankine power plant, where moderated efficiency is achieved with a conventional cycle and values higher than 63% are obtained with supercritical cycles. Similar efficiencies are accomplished with the Brayton power cycle and air heat pump, especially over 700 °C at the discharge, although lower energy density is reached.

Brayton supercritical CO₂ power cycles have attracted much interest in CSP technologies to increase power block efficiency, leading to cost reductions [20]. These power cycles achieve high levels of efficiency mainly due to the high density of CO₂ close to its critical point (suction conditions of the compressor) [21]. This allows for a reduction in the turbine inlet temperature (500 °C), resulting in an efficiency of 40% [22], which may be increased up to 50% at 700 °C [23]. Regarding CSP, the current state of technology includes parabolic trough collectors (PTC) and central receivers (CR). The former is a mature technology with a temperature limit of 400 °C when thermal oil is used as heat transfer fluid. The latter improves the power block efficiency by operating at higher temperatures available from the central receiver, using molten salts as heat transfer fluid and storage medium, with a temperature limit of 600 °C [24].

Reverse Brayton supercritical CO₂ cycles are being proposed for PTES. Vinnemeier et al. [25] compared reverse recuperated Brayton cycles using different fluids, including CO₂, and employing the environment as a thermal source within a wide range of high temperatures produced by the heat pump (50–700 °C). After an optimisation process, the results show that exergy efficiency in the heat pump can reach 70% when the high temperature is in the range of 300–600 °C, and the source temperature is elevated. The integration of this heat pump with several conventional power plants, such as steam Rankine, was analysed, resulting in round-trip efficiencies in the range of 50–60%. Tafur-Escanta et al. [26] proposed a recuperated Brayton supercritical CO₂ reversible cycle, i.e., the same is used in both the charge and discharge modes. Molten salts are used as high-temperature storage, whereas pressurised water is used as the low-temperature thermal source, releasing waste heat into the environment. A round-trip efficiency of 80% is reached, with a levelised cost of storage of 116 €/MWh. Some PTES proposals integrate Brayton heat pumps with solar energy (photovoltaic, PV, and CSP). So, Aga et al. [27] analysed a Brayton supercritical CO₂ heat pump coupled to a steam Rankine power cycle using molten salts (565 °C/270 °C) as the thermal energy storage and hot water (15 °C/60 °C) as the heat source. The low temperature of the heat source encourages the use of an electric heater to reach temperatures higher than 465 °C. The heat pump and the electric heater are driven by PV or electrical grid surpluses. A techno-economic optimisation, considering scale economies (20 MW to 100 MW in steam turbines), was carried out, resulting in a range for the heat pump efficiency (COP) from 1.10 to 1.35 and for the steam Rankine cycle of 31% to 45%. The maximum round-trip efficiency was 60%. Footprint estimation of selected configurations was included in the analysis. Mahdi et al. [28] proposed a reverse Brayton heat pump integrated with a steam Rankine power plant, using molten salts as a thermal energy storage system. Different gases were analysed as working fluid for the heat pump, whereas environment and PTC were combined to supply low thermal energy to the heat pump, which is driven by PV. The Brayton cycle was studied in both simple and recuperated layouts. Round-trip efficiency ranged from 43% to 79%.

This work proposes a TI-PTES, using solar-thermal energy as the source and Brayton supercritical CO₂ cycles for both the heat pump and the heat engine. Based on the literature review, both cycles use recuperators, including recompression in the power cycle.

Two molten salt tanks have been chosen for high-temperature storage. The heat pump and heat engine operate between 85 bar and 300 bar, which necessitates the use of printed circuit heat exchangers (PCHE) to withstand such pressure differences. However, they are not suitable for the CO₂/salt heat exchanger in the heat pump and the salt/CO₂ heat exchanger in the heat engine due to potential clogging issues with the salt inside the narrow channels [29]. This problem was overcome by shifting such heat exchangers to the low-pressure side of each cycle, thus allowing the use of shell and tubes heat exchangers with the salt flowing inside the shell. This modification has been proposed by authors for concentrated solar power plants [30]. A low-temperature storage system, also based on two-tank molten salt storage, has been included to manage the mismatch between solar-thermal production and grid surpluses. The solar field has been sized, taking the concentrated solar plants currently installed in Spain without thermal storage as a reference, whose design power is 50 MWe [31]. The size of the system, performance, and possible operation strategies are assessed.

2. Methodology

2.1. Concept

Figure 1 shows a conceptual diagram of a TI-PTES system. Solar thermal collectors generate a low-temperature source (LTS), whose energy is enhanced by a heat pump (HP) and stored in the high-temperature thermal energy storage (HTTES) during the charge period. In the discharge period, high-grade thermal energy is taken from the HTTES by the heat engine (HE). It is converted into electricity and injected into the grid, and heat is released into the environment (0). The energy balance in the heat pump is shown in Equation (1), whereas Equation (2) shows the energy balance in the heat engine. Thermal energy is represented by Q , electricity by W , subscript $P2S$ stands for “power-to-storage”, i.e., the power taken from the grid, and subscript $S2P$ stands for “storage-to-power”, i.e., the power obtained from the thermal energy stored in the high-temperature storage. The coefficient of performance (COP) of the heat pump is shown in Equation (3), and the energy efficiency of the heat engine (η_{HE}) in Equation (4). The round-trip (power-to-power) efficiency (η_{rt}) is given in Equation (5).

$$Q_{LTS} + W_{P2S} = Q_{HTTES} \quad (1)$$

$$Q_{HTTES} = W_{S2P} + Q_0 \quad (2)$$

$$COP = \frac{Q_{HTTES}}{W_{P2S}} \quad (3)$$

$$\eta_{HE} = \frac{W_{S2P}}{Q_{HTTES}} \quad (4)$$

$$\eta_{rt} = \frac{W_{S2P}}{W_{P2S}} = COP \cdot \eta_{HE} \quad (5)$$

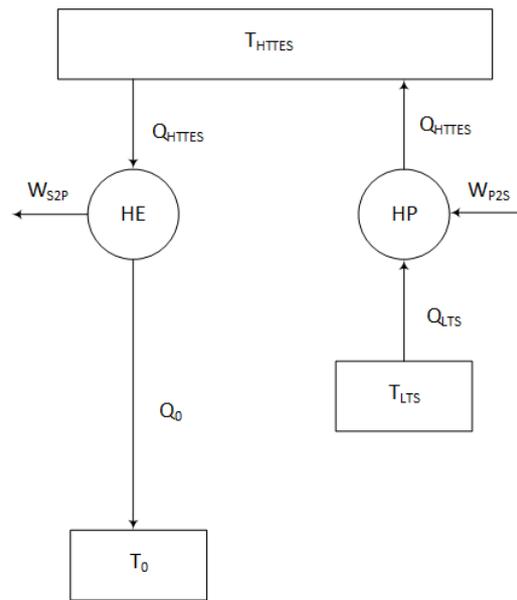


Figure 1. Conceptual diagram of a thermally integrated pumped thermal energy storage (TI-PTES) or Carnot Battery.

Considering the restrictions derived from the Second Law, Equations (6)–(8) give the maximum efficiency of the systems where subscript *max* stands for the maximum value. As is shown by Equation (8), the maximum round-trip efficiency is maximised when the temperature of the cold reservoir is high and close to the temperature of the hot storage, which encourages the use of suitable waste heat sources. One way forward to achieve this suitable low-temperature source is to use linear collectors (parabolic trough or Fresnel) as a compromise between temperature and cost. In this way, T_{LTS} might reach about 600 K. Considering 766 K as T_{HTTES} and 300 K as ambient temperature, the maximum COP reaches 4.61 and the maximum heat engine efficiency 60.8%, resulting in a maximum round-trip efficiency of 281% (electrical energy discharged is 2.81 times the charged). This value means that the heat pump takes from the solar field 3.61 times the energy taken from the grid, thus allowing it to discharge more power into the grid than the one taken in the charge period. Consequently, the thermal integration of the heat pump with the solar field plays a paramount role in the system, allowing it to reach high values of round-trip efficiency. On the other hand, Equation (8) shows that in a simple PTES system, that is, when no low-temperature source is integrated ($T_{LTS} = T_0$), the maximum round-trip efficiency is 100%.

Except for the solar field, the model has been implemented in Engineering Equation Solver (EES) [32]. Carbon dioxide (in the heat pump and the heat engine) and water (as a cooling medium of the heat engine) have been considered pure substances. This way of modelling the CO_2 retains its behaviour at low temperatures, close to its critical point or at high temperatures, more similar to an ideal gas. On the other hand, thermal oil (in the solar field) and molten salt are modelled as incompressible fluids.

$$COP_{max} = \frac{T_{HTTES}}{T_{HTTES} - T_{LTS}} \quad (6)$$

$$\eta_{HE,max} = 1 - \frac{T_0}{T_{HTTES}} \quad (7)$$

$$\eta_{rt,max} = COP_{max} \cdot \eta_{HE,max} = \frac{T_{HTTES} - T_0}{T_{HTTES} - T_{LTS}} = \frac{\frac{T_{HTTES}}{T_{LTS}} - \frac{T_0}{T_{LTS}}}{\frac{T_{HTTES}}{T_{LTS}} - 1} \quad (8)$$

2.2. Heat Engine

The heat engine is based on a Brayton supercritical CO₂ (S-CO₂) power cycle [21]. The National Renewable Energy Laboratory of the US proposes this type of power cycle for the next generation of concentrated solar power plants [33] due to its compactness and good efficiency for moderate temperatures. These cycles frequently use pressure values larger than 200 bar [34], whereas the low pressure is about 85 bar [35]. Such a pressure difference is usually withstood using printed circuit heat exchangers (PCHEs), a type of bonded plate heat exchanger with narrow channels. These narrow channels exhibit a potential issue related to using molten salts as the working fluid in both high and low-temperature storage systems [29]. To avoid this issue, a modification of this cycle is proposed in [30] by relocating the heating supply downstream of the turbine, which is the low-pressure side. This solution uses a shell and tube heat exchanger where the salts flow through the shell and the CO₂ inside the tubes. Figure 2 shows the conventional (a) and the modified (b) layouts.

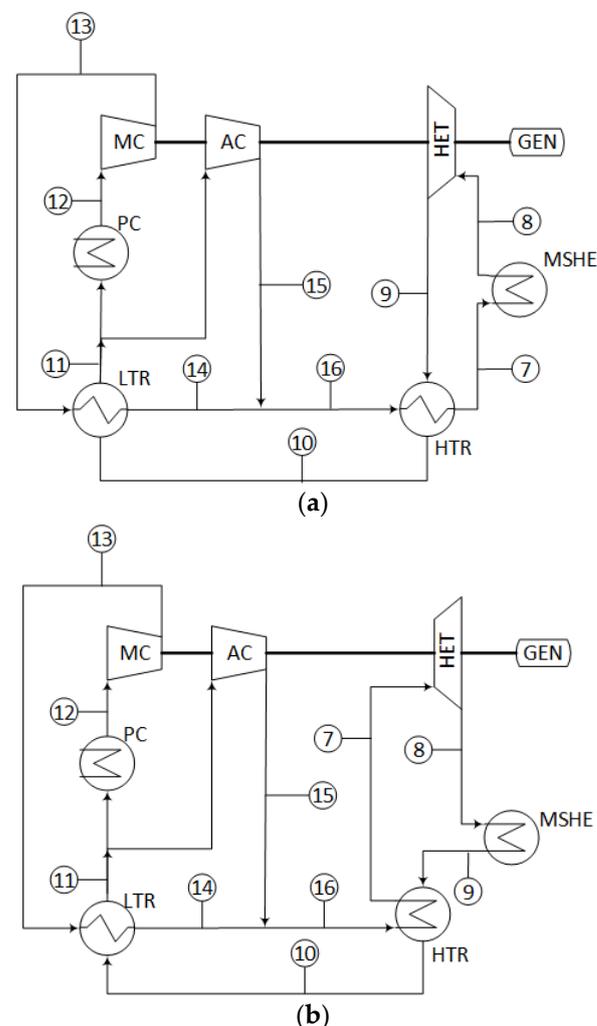


Figure 2. Power cycles (heat engines) recompression layouts: (a) Conventional; (b) Modified.

High efficiencies achieved by S-CO₂ power cycles [21] are based on the closeness of the compressor inlet to the critical point (31.1 °C and 73.8 bar), thus reducing the compression work. Such closeness might produce substantial variations in density, which can be moderated by selecting the compressor inlet pressure at 85 bar, thus maintaining a trade-off between its stable operation and reduced compression consumption [30]. Another issue that may occur in the compressor is phase-change phenomena derived from

local flow accelerations. Operation in the two-phase region can affect the compressor performance and produce erosion and degradation of some parts. To prevent premature power cycle malfunctions, it is imperative to meticulously design the main compressor, taking into account the mentioned challenges.

Moreover, the closeness to the critical point also entails another issue in a simply recuperated Brayton cycle. The specific heat of CO₂ at the low-pressure stream in the recuperator is lower than the one in the high-pressure stream, thus producing an unbalanced profile of temperatures which avoids obtaining the maximum performance of the recovery process. This issue is well known and solved by partitioning the recuperator into two units, leading to the so-called re-compression cycle [21].

Analysing Figure 2b, which represents the heat engine used in the present work, the CO₂ leaving the turbine (HET) takes the thermal energy from the molten salts in the molten salts/CO₂ heat exchanger (MSHE) (8-9) and transfers it to the cold stream (16-7) in the high-temperature recuperator (HTR), reaching the condition of the turbine inlet. Once the hot stream has left the HTR, it transfers thermal energy again (10-11) in the low-temperature recuperator (LTR) to the cold stream (13-14). It can be observed that the cold mass flow rate in the LTR (high-pressure stream) is lower than the mass flow rate of the hot stream (low-pressure steam). This is a key factor in re-compression cycles, pursuing balance in the LTR, as the high-pressure stream exhibits higher specific heat than the low-pressure stream, as mentioned before. The mass flow rate division is done in the inlet (11) of the precooler (PC). After the splitting, the main flow is cooled (11-12) and compressed (12-13) in the main compressor (MC), whereas the rest of the flow (14-15) is sent directly to the auxiliary compressor (AC). As this stream is compressed without previous cooling, it reaches a suitable temperature to be mixed with the cold stream that leaves the LTR (14-15-16) to constitute the cold stream entering the HTR.

The isentropic efficiency of the turbine was set to 92%, and for both compressors we assumed a value of 88% [34]. The temperature approach in HTR was taken as 5 K and in LTR as 5.5 K. The approach temperature in the MSHE was set to 10 K. The main compressor outlet pressure is 300 bar, with 35 °C and 85 bar at its inlet. Pressure drops of 50 kPa were considered in each stream of the heat exchangers [30].

2.3. Heat Pump

A reverse Brayton cycle with supercritical CO₂ as a working fluid was also chosen for the heat pump. This choice aims to design a high-temperature heat pump that takes heat from 300 °C to 400 °C (produced by the solar field) and delivers it between 400 °C to 600 °C. The thermal energy in both cases is exchanged with molten salts. Thus, a sensible heat transfer profile is desirable in the working fluid of the heat pump. For these reasons, a reverse Brayton cycle was selected. As in the heat engine case, PCHes are the best option for the conventional cycle. However, in this study, they were replaced by shell and tube heat exchangers in the absorbing and delivering heat processes to overcome clogging issues with the salts. Figure 3 shows a conventional recuperated reverse Brayton cycle (Figure 3a) and the modified version adopted in the current project (Figure 3b), where both molten salt heat exchangers (LTMS and MSHP) are in the low-pressure side of the cycle due to the allocation of the MSHP upstream the compressor. Remarkably, the conventional reverse Brayton cycle is a simple recuperated one, without re-compression. It operates far from the critical point, so a nearly ideal gas behaviour is expected. This hypothesis is checked later using the property diagrams of the cycle.

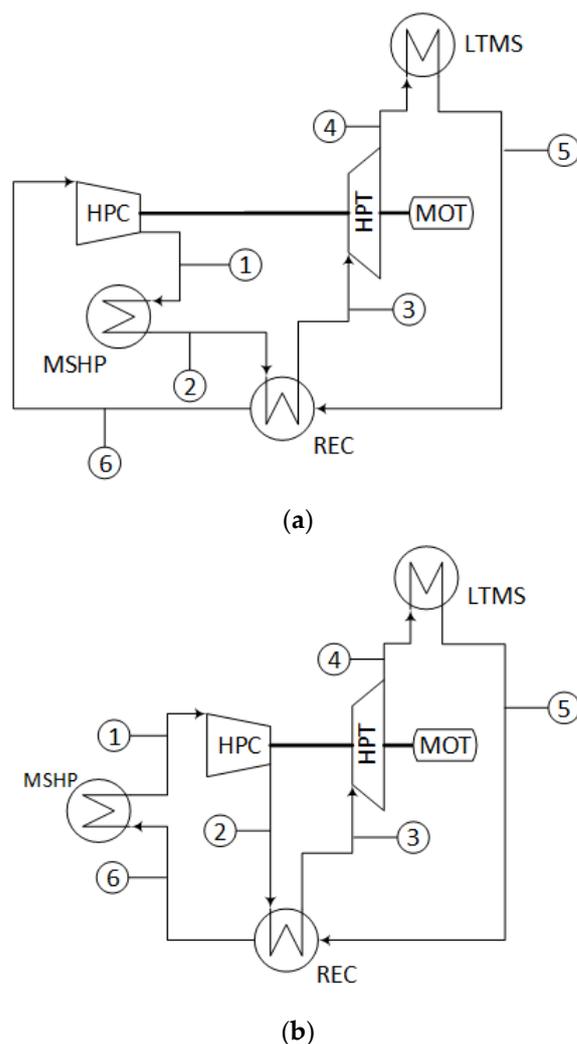


Figure 3. Reverse Brayton cycles (heat pumps) layouts: (a) conventional; (b) modified.

The description of the cycle is as follows: the low-pressure and low-temperature stream (4) leaving the turbine (HPT) takes heat from the low-temperature reservoir in the molten salts/CO₂ heat exchanger (LTMS). A second stage of heating occurs (5–6) in the recuperator (REC), taking advantage of the high temperature of the stream leaving the compressor (2–3). Then, the low-pressure stream, at high temperature after these two heating stages, supplies thermal energy to the hot sink (6–1) through the CO₂/molten salt heat exchanger (MSHP). After that, the low-pressure stream is suctioned by the compressor (HPC), increasing its pressure and temperature (1–2). After the compressor, the high-pressure stream releases heat in the recuperator (2–3), reaching the turbine inlet conditions (3).

The isentropic efficiency of the turbine and the compressor were set to 92% and 88%, respectively. The temperature approach in the recuperator was taken as 5 K. The approach temperature in the low-temperature molten salts/CO₂ heat exchanger was set to 10 K. The compressor outlet pressure is 300 bar, with 415 °C and 85 bar at the inlet. Pressure drops of 50 kPa were considered in each stream of the heat exchangers [30].

2.4. Molten Salts Loops

Two molten salt loops were included in the system, shown in Figure 4. The high-temperature loop (Figure 4a) stores the thermal energy at a suitable temperature to be converted into electricity by the heat engine in the discharge period. The low-temperature loop (Figure 4b) was introduced to prevent a mismatch between the solar resource and

surplus power in the grid. Thus, thermal energy from the solar field might be eventually stored, waiting for a power surplus in the grid to drive the heat pump.

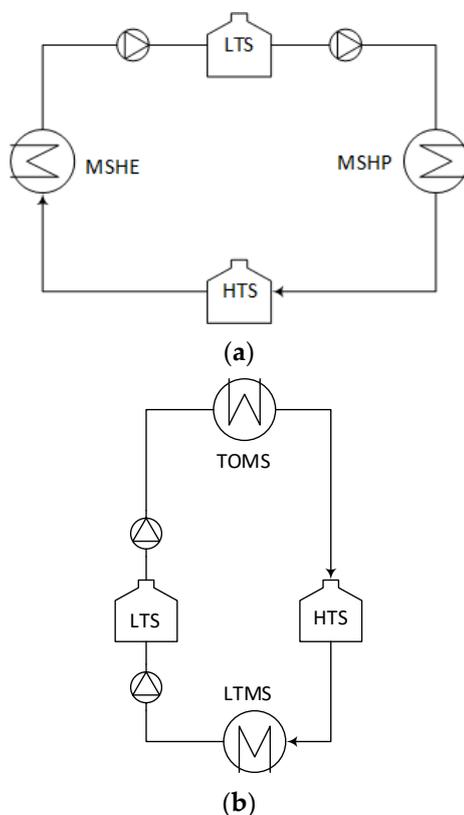


Figure 4. Molten salt loops: (a) high temperature; (b) low temperature.

Solar salt (whose weight composition is 60% NaNO_3 and 40% KNO_3) was chosen as the working fluid, at 589 °C/405 °C in the tanks of the high-temperature loop (HTS and LTS, respectively) and 380 °C/290 °C in the low-temperature loop (HTS and LTS tanks, respectively). The molten salt proposed and the range of temperatures of the high-temperature tanks are similar to CSP's current state-of-the-art, based on central receivers. The range of temperatures of the low-temperature tanks can be found in the current CSP, based on parabolic troughs with storage [36]. So, no corrosion or any other material-related issues are expected to occur different from those that have already been observed at CSP plants with storage.

The approach temperature in the thermal oil/molten salt heat exchanger (TOMS) was set to 10 K. Pressure drops in molten salts were considered only in the heat exchangers. The consumption of the pumps was neglected.

2.5. Solar Field

The solar field consists of parabolic trough collectors using Therminol VP1 [37] as heat transfer fluid, which is a proven and mature technology for the temperature range considered [37].

For the sizing and nominal performance of the solar field, the design point was set on the 21st of June at solar noon, at Seville (Spain), with direct normal irradiation (DNI) equal to 900 W/m^2 . The type of parabolic trough collector used is the Eurotrough, as shown in Table 2 [31]. The heat loss correlation used to calculate the thermal performance is provided by the manufacturer [38].

Table 2. Geometric and optical parameters of the solar field [31].

Number of loops in the solar field	78
Number of collectors per loop	4
Number of modules per collector	10
Length of every module (m)	12.27
Absorber tube outer diameter (m)	0.07
Absorber tube inner diameter (m)	0.065
Glass envelope outer diameter (m)	0.115
Glass envelope inner diameter (m)	0.109
Intercept factor	0.92
Mirror reflectivity	0.92
Glass transmissivity	0.945
Solar absorptivity	0.94
Peak optical efficiency	0.75

As shown in Table 2, the total number of loops is 78, each consisting of 4 collectors with 10 modules, with a total loop length equal to 490.8 m. The main parameters characterising the nominal performance of each loop are summarised in Table 3.

Table 3. Nominal performance of the parabolic trough loop.

Mass Flow per loop (kg/s)	7.6
Inlet/Outlet HTF temperature (°C)	300/390
Inlet Pressure (bar)	20
Heat gain per loop (MWth)	1.6732
Heat loss per loop (kWth)	158.56
Pressure drop per loop (bar)	4.1438
Optical efficiency (%)	71.99
Thermal efficiency (%)	91.34

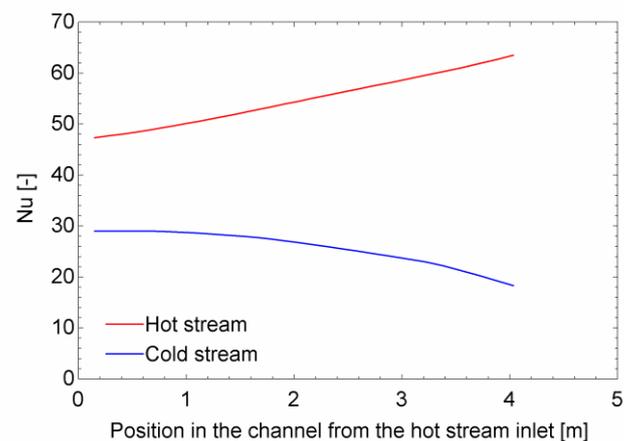
2.6. Sizing of Heat Exchangers

Two types of heat exchangers were used: printed circuit heat exchangers (PCHE) and shell and tube heat exchangers (STHE). As mentioned before, the former is commonly used in S-CO₂ to withstand high-pressure differences; the latter is used when molten salt is one of the fluids to avoid clogging issues [30].

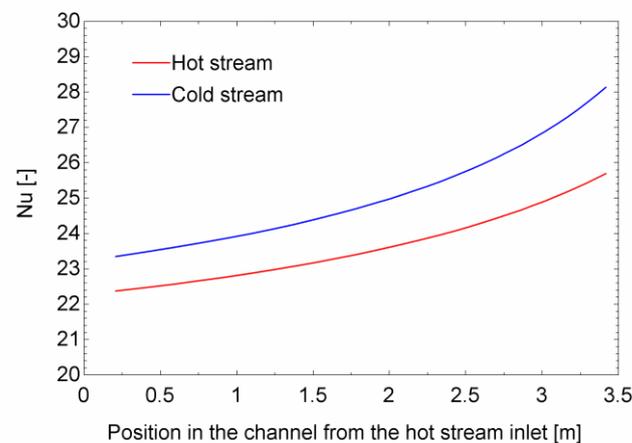
The sizing of the PCHEs is highly influenced by the wide variation of CO₂ properties, mainly when the working conditions are close to the critical point. This requires an iterative design method based on sub-heat exchangers. A continuous variation of properties was assumed along the different sub-heat exchangers that constitute the entire unit [39]. According to the leading manufacturer [40], the maximum plate size is 600 × 1500 mm. Plates were assembled in modules with a core block assumed to have a maximum height of 600 mm, which entails a total number of 96,000 channels (48,000 per stream). This design was taken from the manufacturer [41] and was employed in a previous work with CSP technologies [30]. Up to 14 modules can be stacked in parallel in a bonding structure, constituting the largest stack (8.4 m long) [30]. The flow channels are 2 mm semicircles with a 2.5 mm pitch, and each plate has a thickness of 1.6 mm. Due to the high temperatures, Inconel alloy 617 was recommended for both REC and HTR [42]. Austenitic stainless steel 316L was selected for the rest of the PCHEs.

For each sub-heat exchanger, the overall heat transfer coefficient was evaluated by combining the convection heat transfer coefficients of both streams with the thermal conductance per unit heat transfer area between their channels, following the methodology described by Dostal [21]. The heat transfer through the surface area of the heat exchanger was then used to determine its length as a function of its perimeter. The pressure drop along the entire channel could then be evaluated for every stream. The iterative design procedure started with an initial guess of the number of channels and proceeded to assess each sub-heat exchanger until the prescribed temperatures at each of their ports were reached. The total length achieved was then used to determine the maximum pressure drop between both streams. If this maximum pressure drop is greater or lower than the prescribed value, the number of tubes is increased or decreased, respectively.

To better understand how the properties of the PCHes vary, Figure 5a shows the Nusselt number (Nu) along the heat exchanger for both streams of the LTR (close to the critical point). Figure 5b shows the same information for the REC (far from the critical point). It can be appreciated how the low temperature and proximity to the critical point of the cold stream in the LTR produce a different trend from the other streams. The profiles at the REC, where the operation zone of the CO₂ is expected to behave like an ideal gas, might be assimilated to average values.



(a)



(b)

Figure 5. Nusselt number: (a) LTR (146 MW) in the heat engine; (b) REC (266 MW) in the heat pump.

The heat transfer to the CO₂ in STHE was calculated using the Gnielinski correlation, while the pressure drop is determined using the Darcy–Weisbach equation [43]. Since the working temperatures were far from the critical point, averaged CO₂ properties were considered. For the molten salt in the shell, the McAdams correlation was suggested for calculating the heat transfer, and the Kern method was used to determine the pressure drop [43].

Both the tubes and the shell were proposed to be made of stainless steel A213 Gr 347, as it is recommended for its compatibility and cost-effectiveness [33]. These STHEs are modelled as counterflow heat exchangers with one shell pass and one tube pass, except for the TOMS (thermal oil/molten salt), which uses two passes in both shell and tubes. An “E” shell type was selected according to Tubular Exchanger Manufacturers Association (TEMA) standards [44]. The minimum tube thickness is calculated according to the ASME Boiling and Pressure Vessel Code [45]. A standardised wall thickness was selected based on this lower limit and the Birmingham Wire Gage (BWG) of the tube. Other manufacturing requirements were also considered. The shell-diameter-to-tube-length ratio should be within the limits of 1/5 to 1/15. Additionally, architectural layouts and transportation constraints limited the maximum tube length to about 40 m.

2.7. Economic Model

The investment cost (fixed capital investment, FCI, according to [46]) was estimated. This cost is divided into direct and indirect costs, with the latter taken as 25% of the former. Direct costs are composed of on-site costs (equipment, piping, instrumentation, and controls) and off-site costs (land, civil works, and service facilities). Indirect costs include engineering and supervision, construction, and contingencies. In this work, the off-site costs were included in the solar field and the storage systems, whose investment is directly the direct cost. The rest of the facility was assessed from the purchased equipment cost (PEC), obtaining the on-site cost when multiplying it by 2.18 [47].

For the estimation of the heat engine and heat pump (both with Brayton supercritical CO₂ cycles), a study from Sandia National Laboratory [47] for a recompression cycle of 10 MWe was taken as a basis.

The PCHEs were scaled using the number of modules, being the manufacturing unit. The escalation factor is 0.4 [46], the base PEC is USD 5 M with several modules of 4.46 for the HTR and REC, and USD 3 M and 3.1, respectively, for the rest of the PCHEs (data from 2013, [47]). The reason is that the HTR and REC operate at temperatures that demand the use of Inconel 617 alloy, whereas the other heat exchangers are manufactured in SS 316 [48].

Investment in turbomachinery, the generator in the heat engine and the motor in the heat pump were scaled according to Equations (9)–(12), taken from [49].

$$f_w = \left(\frac{W}{10 \text{ MW}} \right)^{0.68} \quad (9)$$

$$f_p = \left(\frac{p}{200 \text{ bar}} \right)^{-0.6} \quad (10)$$

$$f_T = \frac{3.35 + \left(\frac{T[^\circ\text{C}]}{1,000} \right)^{7.8}}{3.35 + \left(\frac{650 \text{ }^\circ\text{C}}{1,000} \right)^{7.8}} \quad (11)$$

$$PEC_{TMG} = f_w \cdot f_p \cdot f_T \cdot 6 \text{ M\$} \quad (12)$$

The PEC for STHEs was estimated using the Purohit method [50]. The cost of the heat exchanger was determined based on the cost of a baseline heat exchanger, which was adjusted by taking into account various factors, such as different materials, pressures, and

other design features. The cost, C_E (USD), was estimated using Equation (13), supported by Equation (14). Here, C_b represents the cost of the baseline heat exchanger made of a base material (carbon steel) ($\$/\text{ft}^2$) designed for a specific pressure range (cost based on 1982 data). D_{Sh} is the shell's inside diameter (in), p is a cost multiplier for the tube outside diameter, pitch, and layout angle, f is a cost multiplier for the TEMA-type front head, and r is a cost multiplier for the TEMA-type rear head. C_i represents the factors that adjust the base cost due to the differences from the reference heat exchanger [50], and A is the heat transfer area (ft^2).

The cost estimation for the thermal energy storage systems was derived from the NREL Gen3 roadmap for CSP [33], with a two-tank solar salt system from Abengoa as a basis. The costs are reported as direct costs, that is, including both on-site and off-site expenses. The volume of the cold tank was taken as the base value ($15,700 \text{ m}^3$), and the escalation factor is 0.8. The cold tank's base cost is USD 4.361 M, the hot tank's is USD 10.016 M, the structural steel's is USD 0.666 M, instrumentation's is USD 0.212 M, the tank insulation's is USD 3.724 M, electrical installations' is USD 0.481 M, the foundations' is USD 3.050 M, and the site works' is USD 0.339 M. The salt inventory cost varies linearly, with a specific cost of USD 1100/tonne. The investment cost for the solar field was estimated, considering a specific cost of USD 152/ m^2 per solar aperture area (with reference to 2020) [51].

To update data from different dates, time scalation using the Chemical Engineering Plant Cost Index (CEPCI) was performed. The CEPCI in 1982 (STHE) was taken as 314, in 2013 (molten salts loops, PCHEs, and turbomachines) as 567.3, and in 2020 (date when results have been referred to) as 596.2.

$$C_E = C_b \cdot \left(1 + \sum_i C_i \right) \cdot A \quad (13)$$

$$C_b = \left[\frac{6.6}{1 - e^{((7-D_{Sh})/27)}} \right] \cdot p \cdot f \cdot r \quad (14)$$

Once the investment had been determined, a preliminary value for the levelised cost of storage (LCOS) was carried out. It was assumed that the electricity to drive the heat pump comes from grid surpluses, with a cost set to zero. Furthermore, maintenance costs were also neglected. With these conditions, the LCOS based on discharged energy (assuming 365 cycles of charge/discharge per year) is given by Equation (15), where \dot{W}_{HE} stands for the net power of the heat engine (discharge power), H_{disch} for the discharge hours in a day and CRF is the capital recovery factor (CRF), given in Equation (16). In this equation, $wacc$ stands for the weighted average capital cost, taken as 7.5%, and N is the life span of the project, taken as 25 years.

$$LCOS = \frac{FCI \cdot CRF}{\dot{W}_{HE} \cdot H_{disch} \cdot 365} \quad (15)$$

$$CRF = \frac{wacc \cdot (1 + wacc)^N}{(1 + wacc)^N - 1} \quad (16)$$

3. Results

3.1. Complete Layout

Figure 6 shows the complete layout, including the thermal engine, heat pump, two molten salt loops (high and low temperature), and the solar field (represented by one equivalent solar collector). Tables 4 and 5 show the properties of the state points (heat pump and heat engine, respectively). Regarding the molten salt temperatures, Table 6 shows them in the storage tanks. Regarding the thermal oil in the solar field, the collector outlet temperature is $390 \text{ }^\circ\text{C}$ and the collector inlet temperature is $300 \text{ }^\circ\text{C}$. The novelty of

the proposed system, especially the allocation of the high-temperature molten salt loop heat exchangers in the heat engine and heat pump, makes it impossible to check the results with simulations of other authors. However, the model used in the current work for the heat engine is the same that was used and validated in [30]. Regarding the heat pump, a simplified version was applied to a reverse cycle.

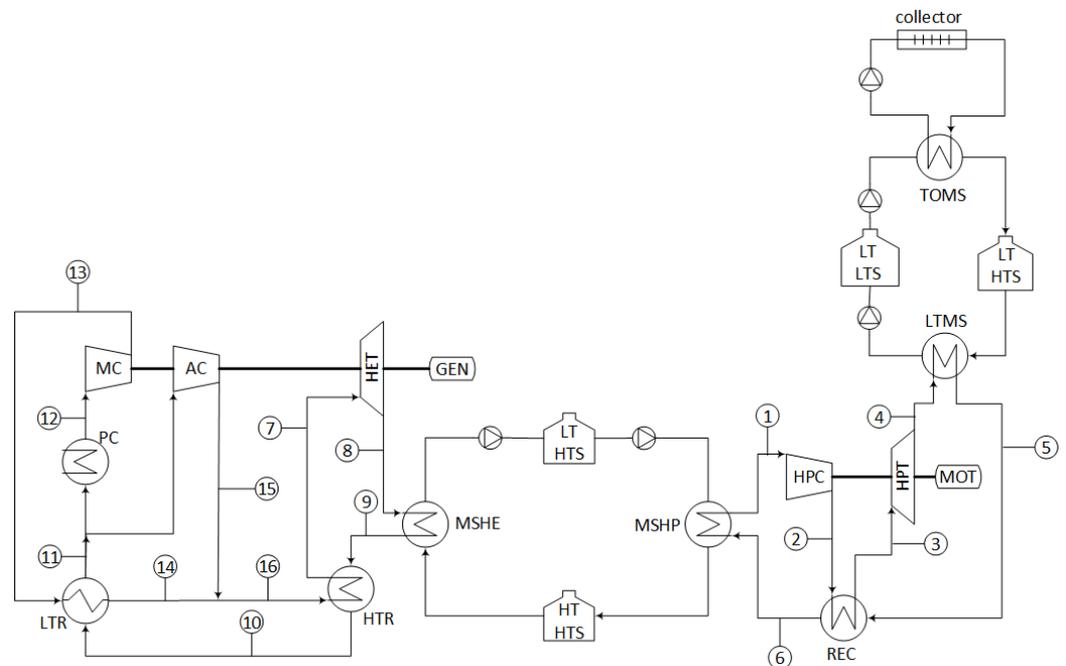


Figure 6. The complete layout of the proposed Carnot battery.

Table 4. Properties at state points (Figure 5) of the heat pump.

Point	Pressure (bar)	Temperature (°C)	Enthalpy (kJ/kg)
1	85.00	415.0	377.28
2	300.0	604.1	590.78
3	299.5	389.2	318.67
4	86.50	256.0	194.39
5	86.00	370.0	324.89
6	85.50	599.1	597.00

Table 5. Properties at state points (Figure 5) of the heat engine.

Point	Pressure (bar)	Temperature (°C)	Enthalpy (kJ/kg)
7	299.0	532.9	500.51
8	87.00	385.4	342.50
9	86.50	579.1	572.58
10	86.00	207.2	138.99
11	85.50	82.02	-17.394
12	85.00	35.00	-197.94
13	300.0	76.52	-163.33
14	299.5	201.7	66.166
15	299.5	203.3	68.548
16	299.5	202.2	66.925

Table 6. Temperatures of storage tanks in the molten salt loops (Figure 5).

Loop	Hot Tank Temperature (HT) (°C)	Cold Tank Temperature (LT) (°C)
High temperature (HTS)	589	405
Low temperature (LTS)	380	290

Figure 7 shows the pressure–enthalpy diagram of both the heat pump and heat engine, with each turbomachine process identified. It is worth pointing out that the compression processes in the heat engine show steeper slopes, particularly in the main compressor, due to their closeness to the critical point. However, the behaviour of the heat pump can be assimilated to a pure reverse Brayton cycle, that is, operating with an ideal gas. Figure 8a shows the heat pump cycle, whereas Figure 8b displays the heat engine cycle, both with heat exchanger identifications. In Figure 8b, the LTR enthalpy change exhibits a different length between the high and low-pressure streams (longer at the high-pressure stream). This is due to the lower mass flow ratio in the former, which compensates for its higher specific heat.

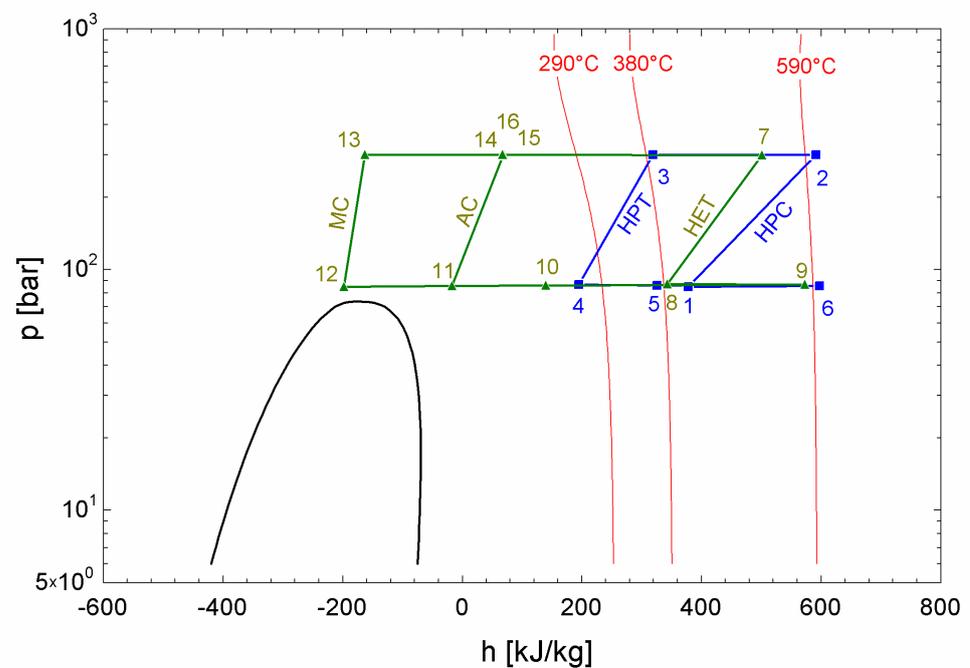
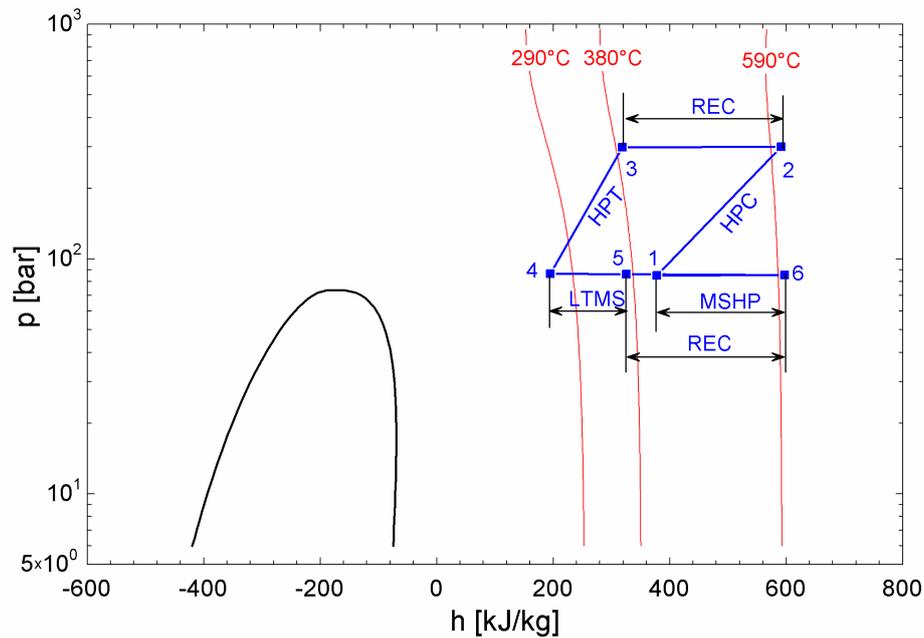
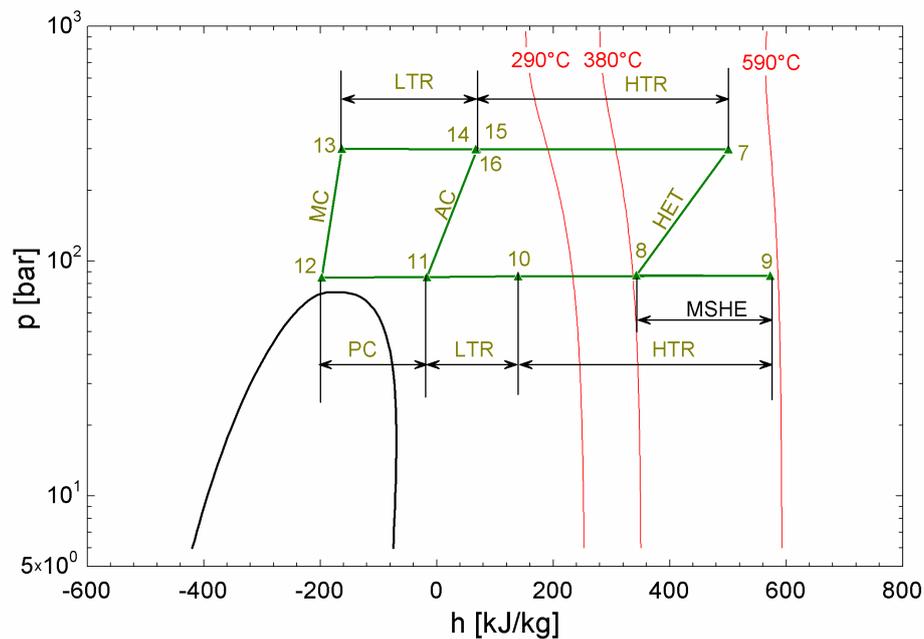


Figure 7. Pressure–enthalpy diagram of the proposed Carnot battery (heat pump in blue lines and heat engine in green lines).



(a)



(b)

Figure 8. Pressure–enthalpy diagrams: (a) heat pump; (b) heat engine.

The design point was set for charge and discharge periods with the same duration for both thermal storage systems as if they were working instantaneously. At this design point, the heat engine was assumed to produce 100 MWe. The charge and discharge periods were characterised by their number of hours (H_{ch} and H_{disch} , respectively). Regarding the solar resource, the energy collected was equally distributed over constant heat duty in the so-called equivalent hours of solar resource (H_{sres}), accounting for variations in solar radiation. As previously explained, the low-temperature molten salt loop helps to overcome any mismatch between solar resources and grid surpluses.

The pump multiple (PM) is a factor that modulates the design size of the heat pump components according to the solar resource and charge periods, as expressed in Equation (17). Similarly, the engine multiple (EM) is a factor that modulates the design size of the heat engine components according to the solar resource and discharge periods, as expressed in Equation (18).

$$PM = \frac{H_{sres}}{H_{ch}} \quad (17)$$

$$EM = \frac{H_{sres}}{H_{disch}} \quad (18)$$

Tables 7 and 8 give the energy balances in both the heat pump and the heat engine, respectively. These tables include the multipliers previously defined, which will be set according to the strategy of operation (choice of charge and discharge period length).

Regarding the solar field, the heat duty of the thermal oil/molten salts heat exchanger (TOMS) was 128 MW and the mass flow rate of the thermal oil was 592.8 kg/s, both without any multiplier.

Table 7. Energy balance at the design point of the heat pump (Figure 6). In the HE, the hot stream is designed in the first place.

Component	Heat Duty or Power (MW)	Mass Flow Rate (kg/s)
Compressor (HPC)	209 PM	978 PM
Turbine (HPT)	122 PM	978 PM
Motor (MOT)	87 PM	---
CO ₂ /CO ₂ (REC)	266 PM	978 PM/978 PM
Molten salts/CO ₂ (LTMS)	128 PM	941 PM/978 PM
CO ₂ /Molten salts (MSHP)	215 PM	978 PM/761 PM

Table 8. Energy balance at the design point of the heat engine (Figure 6). In the HE, the hot stream is designed in the first place.

Component	Heat Duty or Power (MW)	Mass Flow Rate (kg/s)
Main Compressor (MC)	22 EM	637 EM
Auxiliary Compressor (AC)	26 EM	297 EM
Turbine (HET)	148 EM	934 EM
Generator (GEN)	100 EM	---
CO ₂ /CO ₂ (HTR)	405 EM	934 EM/934 EM
CO ₂ /CO ₂ (LTR)	146 EM	934 EM/637 EM
Molten salts/CO ₂ (MSHE)	215 EM	761 EM/934 EM
CO ₂ /Water (PC)	115 EM	637 EM/5502 EM

3.2. Performance

Considering the energy balances given in Tables 7 and 8, the performance of the system is represented by Equations (19)–(21). A round-trip efficiency higher than one is reached thanks to the high COP achieved by enhancing the low-temperature source with the solar collector.

Assuming incompressible behaviour for the molten salts and cooling water, the entropy average temperature of each storage and the sink is given by Equations (22)–(24) [52]. Replacing these values in Equations (6)–(8), a maximum roundtrip efficiency of 2.92 was achieved. If both multipliers are taken as one (design case), per each hour of the solar resource, the energy input consists of 128 MWhth from the solar field and 87 MWhth

charged from grid surpluses. The energy output includes 100 MWh discharged into the grid, and 115 MWh rejected to the cooling water.

$$COP = \frac{215 \cdot PM \cdot H_{ch}}{87 \cdot PM \cdot H_{ch}} = \frac{215 \cdot H_{sres}}{87 \cdot H_{sres}} = 2.47 \quad (19)$$

$$\eta_{HE} = \frac{100 \cdot EM \cdot H_{disch}}{215 \cdot EM \cdot H_{disch}} = \frac{100 \cdot H_{sres}}{215 \cdot H_{sres}} = 0.4651 \quad (20)$$

$$\eta_{rt} = \frac{100 \cdot H_{sres}}{87 \cdot H_{sres}} = COP \cdot \eta_{HE} = 1.15 \quad (21)$$

$$T_{LTES} = \frac{380 - 290}{\ln\left(\frac{380 + 273}{290 + 273}\right)} = 606.89 \text{ K} \quad (22)$$

$$T_{HTES} = \frac{589 - 405}{\ln\left(\frac{589 + 273}{405 + 273}\right)} = 766.32 \text{ K} \quad (23)$$

$$T_0 = \frac{30 - 25}{\ln\left(\frac{30 + 273}{25 + 273}\right)} = 300.49 \text{ K} \quad (24)$$

The multipliers allow covering any strategy of operation. Some examples are given in Table 9. In all the cases, the solar resource period was taken as 6 h and the solar field produced 128 MW at its design point. In the case that surpluses are due to photovoltaic production (PV), a shorter charge period is expected, assumed as 3 h; if the surpluses are due to wind generation (WF), which usually occurs at night, a charge period of 6 h is proposed. Regarding the discharge periods, depending on the demand, one (1 pk) or two peaks (2 pk) periods can occur.

Table 9. Operation strategies according to the surplus origin and demand profile for 6 equivalent hours of the solar resource. Charge power (heat pump consumption) and discharge power (heat engine production) are calculated for a solar field of 128 MW.

Surplus Origin	H_{ch}	Demand Profile	H_{disch}	PM	EM	Charge Power (MW)	Discharge Power (MW)
PV	3	1 pk	3	2	2	174	200
	3	2 pk	6	2	1	174	100
WF	6	1 pk	3	1	2	87	200
	6	2 pk	6	1	1	87	100

The main dimensions and on-site costs of HEs at different configurations of surplus origin and demand profile are given in Table 10 for PCHE and in Table 11 for STHE. Table 12 shows the on-site cost for the set of turbomachines and electrical machines (motor and generator) according to the surplus origin (heat pump) and demand profile (heat engine). Table 13 displays the direct costs of molten salt loops and solar fields. Finally, Table 14 combines the previous values according to the four configurations analysed, determining the investment and the levelised cost of storage of each one.

Table 10. Size and costs of PCHE at different configurations.

Component	Profile	Heat Duty (MW)	Height (m)	Number of Modules	On-Site Cost (USD M ₂₀₂₀)
REC	WF	266	3.42	128	43.9

	PV	532	3.42	256	57.9
HTR	2 pk	405	2.38	59	32.2
	1 pk	810	2.38	118	42.5
LTR	2 pk	146	4.03	99	27.5
	1 pk	292	4.03	198	36.2
PC	2 pk	115	0.54	10	10.8
	1 pk	230	0.54	20	14.2

Table 11. Size and costs of STHE at different configurations.

Component	Profile	Heat Duty (MW)	Length (m)	Shell Diameter (m)	Number of Units	On-Site Cost Per Unit (USD M ₂₀₂₀)
TOMS	All	128	30.2	3.18	1	35.6
LTMS	WF	128	14.8	3.62	1	67.6
	PV	256	14.8	3.62	2	135
MSHP	WF	215	39.5	4.26	1	286
	PV	430	39.5	4.26	2	572
MSHE	2 pk	215	30.2	4.05	1	191
	1 pk	430	30.2	4.05	2	382

Table 12. Turbomachines and electrical machine costs for different configurations.

Cycle	Type	On-site Cost (USD M ₂₀₂₀)
HP	WF	20.4
	PV	32.7
HE	2 pk	22.4
	1 pk	35.9

Table 13. Molten salt loops and solar field costs.

Component	Energy Stored (MWh)	Salt Inventory (ton)	Direct Costs (USD M ₂₀₂₀)
LTS	768	20,393	44.0
HTS	1290	16,462	37.0
Solar Field	---	---	32.5

Table 14. Fixed capital investment and levelised cost of storage at different configurations.

Surplus Origin	Demand Profile	Discharge Power (MW)	Discharge Energy (MWh)	FCI (USD M ₂₀₂₀)	LCOS (USD ₂₀₂₀ /MWh)
PV	1 pk	200	600	1,865	639
	2 pk	100	600	1,571	538
WF	1 pk	200	600	1,392	477
	2 pk	100	600	1,098	376

4. Discussion and Conclusions

A Carnot battery was proposed based on Brayton supercritical CO₂ thermodynamic cycles. The architecture corresponds to a thermal integrated pumped thermal energy storage (TI-PTES). The thermal source was supplied by a solar field constituted of parabolic trough collectors, which allowed reaching an entropy average temperature of 334 °C. To overcome the possible mismatch between grid surpluses and the solar resource, a low-

temperature thermal energy storage system based on a two-tank solar salt system was provided. Another two-tank system with the same molten salts was allocated to store the heat enhanced by the heat pump and consumed by the heat engine. This second storage system operates as a thermal reservoir at 493 °C (entropic average temperature). The thermal sink is a cooling water system with an entropic average temperature of 27.5 °C. With these thermal boundaries, a round-trip efficiency of 2.92 would be reached if all the systems operated totally reversibly. The proposed system achieves a round-trip efficiency of 1.15, far from the reversible case but higher than the usual storage systems [1]. Common PTES system efficiencies, without enhanced thermal sources, go down below 70% [15].

The performance of the system depends on its ability to maximise the use of thermal sources within realistic boundary restrictions. In this sense, current state-of-the-art of CSP technology parameters have been selected, and their economic impact has been evaluated. An exergy analysis is proposed in Equations (25) and (26) for the heat pump and 27 to 28 for the heat engine. In these equations, I stands for the overall irreversibility of each system and η_{II} represents the second law of efficiency, i.e., the ratio of exergy recovered to the exergy supplied [52]. It can be observed that the exergy conversion of each system is highly efficient, with more than 2/3 of the exergy recovered in the heat pump and more than 3/4 in the heat engine. The exergy efficiency of the heat pump is in line with [25], which suggests that a maximum temperature of 300–600 °C and an elevated source temperature can achieve 70% efficiency. The heat engine's exergy efficiency is consistent with these types of cycles [22].

$$Q_{LTS} \cdot \left(1 - \frac{T_0}{T_{LTS}}\right) + W_{P2S} = Q_{HTTES} \cdot \left(1 - \frac{T_0}{T_{HTTES}}\right) + I_{HP} \quad (25)$$

$$\eta_{II,HP} = \frac{Q_{HTTES} \cdot \left(1 - \frac{T_0}{T_{HTTES}}\right)}{Q_{LTS} \cdot \left(1 - \frac{T_0}{T_{LTS}}\right) + W_{P2S}} = \frac{COP \cdot \left(1 - \frac{T_0}{T_{HTTES}}\right)}{(COP - 1) \cdot \left(1 - \frac{T_0}{T_{LTS}}\right) + 1} = 67.87\% \quad (26)$$

$$Q_{HTTES} \cdot \left(1 - \frac{T_0}{T_{HTTES}}\right) = W_{S2P} + I_{HE} \quad (27)$$

$$\eta_{II,HE} = \frac{W_{S2P}}{Q_{HTTES} \cdot \left(1 - \frac{T_0}{T_{HTTES}}\right)} = \frac{\eta_{HE}}{\eta_{HE,max}} = 76.51\% \quad (28)$$

The use of the solar field as an alternative to waste heat has allowed us to obtain a high COP in the heat pump. The required size is typical for a CSP of 50 MWe with an efficiency of 38%, without storage, as usual in Spain [53]. In fact, using the grid to power the heat pump allows for avoiding the usual oversizing of the solar field (solar multiple). It also allows allocating the investment to the components of the heat pump and heat engine instead, thus reducing it as it is strongly dependent on the solar collectors [54].

Once the low thermal source has reached a high value, a high-temperature heat pump is required. This challenge was addressed using a reverse Brayton cycle with supercritical CO₂. It is well known that this kind of cycle suits well with intermediate to high temperatures [55], and the turbomachines avoid issues found in compression (VCHP) heat pumps. By shifting the heat-release heat exchanger to the low-pressure side, based on the authors' proposal for heat engines [30], it is possible to use molten salts and high-pressure ratios, thereby increasing efficiency.

The levelised cost of storage ranged from USD 376/MWh to USD 639/MWh. The basic configuration (6 h charging and 6 h discharging) achieved the lowest cost (USD 376/MWh), which is comparable to current Li-ion batteries [26]. However, a cost range of USD 120/MWh to USD 250/MWh is expected in 2030 for batteries. These values indicate that the cost of the proposed system is too high. To find ways to reduce the investment, a cost breakdown is shown in Figure 9. Since all configurations were sized for the same

amount of discharged energy, the lower the operating time, the higher the investment required. Therefore, the highest investment occurs in PV-1pk (3 h charging/3 h discharging) and the lowest in WF-2pk (6 h charging/6 h discharging), with intermediate–high value in PV-2k and intermediate–low value in WF-1k. Figure 9 points out that the most critical cost, by far, is the investment in the shell and tube heat exchangers. Therefore, this should be the first option to explore to achieve a reasonable cost.

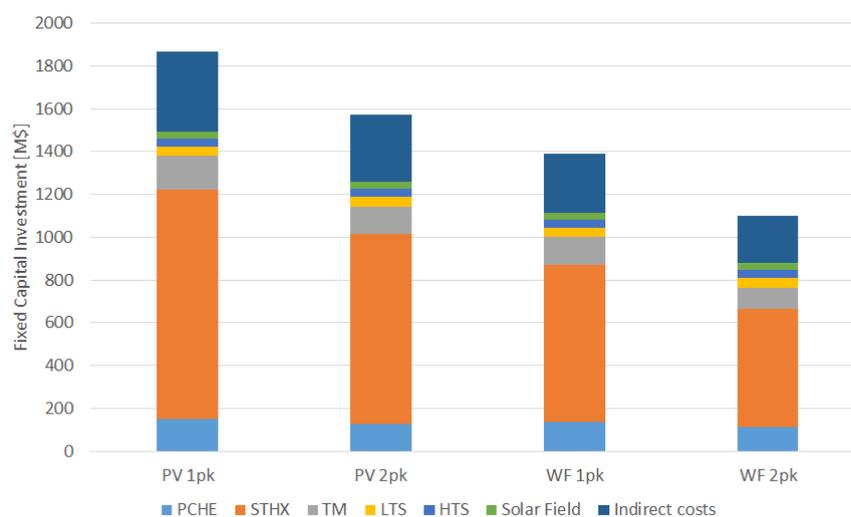


Figure 9. Investment breakdown of different configurations.

The most effective way to reduce investment costs associated with STHE is to replace them with hybrid printed circuit heat exchangers. In this scheme, one stream's layers are replaced with a plate-and-fin structure, thus constituting a hybrid heat exchanger that combines a PCHE and a plate-fin heat exchanger (PFHE). This type of HE has been proposed for sodium fast reactor (SFR) generation IV nuclear reactors, where liquid metal cools the reactor by circulating through the plate-fin structure, and CO₂ flows through the semi-circular channels [56]. These heat exchangers have been available from Heatric since 2006 as hybrid heat exchangers (H²X), manufactured from chemically etched sheets and corrugated fins [57]. In the current proposed application, molten salts would flow through the corrugated fins, and CO₂ would flow through the semi-circular channels. Corrugated fins are expected to withstand pressures of 200–220 bar [57], so allocating H²X in the low-pressure side is suitable for these heat exchangers.

As the proposed H²X is an evolution of the PCHE, it is expected to have a similar cost. Therefore, by considering the overall investment in PCHE for the WF-2pk configuration and replacing the STHE with H²X, an estimation of the new investment can be obtained (USD 550 M), resulting in a levelised cost of storage of USD 188/MWh. The overall heat duty in all the STHEs is lower than in all the PCHEs, so a safety factor is assumed in the previous hypothesis. The resulting cost is consistent with other PTES systems based on Brayton supercritical CO₂ cycles [26] and with current CSP plants without storage (USD 182/MWh) [58]. Hence, once STHEs are replaced by hybrid heat exchangers and an optimisation of the pressure drops is carried out, a reasonable levelised cost of storage is expected.

Solar salts and parabolic trough collectors have been proposed in order to limit investment costs, focusing on the technological challenge in the Brayton supercritical CO₂ cycles. In this sense, the molten salt heat exchangers have been identified as the key cost element, and the hybrid heat exchangers have been proposed as a solution that should be

explored. Once this option is assessed, the next steps in cost reduction will involve optimising pressure drops of printed and hybrid heat exchangers, and finding a trade-off between cost and efficiency. In future works, using a central receiver with a heliostats field might be analysed, replacing the solar salt in the high-temperature loop with a ternary salt [59] to withstand higher temperatures. With such an upgrade, higher efficiencies in both the heat pump and the heat engine are expected, substantially increasing the round-trip efficiency.

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